

CONSTRAINED SEDIMENTATION OF POLYDISPERSED  
PARTICLES IN A CENTRIFUGAL FIELD

E. A. Nepomnyashchii and S. G. Gurevich

UDC 66.065.2

The article presents the results of a study concerning the constrained sedimentation of microparticles in a centrifugal field, treating the kinetics of this process as the kinetics of a random process described by methods analogous to the classical methods of describing the sedimentation of colloidal particles and the Brownian motion in a gravitational field [Smolukhovskii, Einstein, etc.].

Assuming that sedimentation takes place in a cylindrical vessel which revolves at an angular velocity  $\omega$  and disregarding the relativistic as well as the Coriolis forces of inertia, one can describe the sedimentation of particles along the vessel by the following stochastic equation:

$$\frac{dr}{dt} = \frac{2R^2 \left( \frac{\rho}{\rho_s} - 1 \right) \omega^2 r}{9\nu} + \frac{1}{6\pi\rho_s \nu R} \xi(t),$$

where  $R$  is the equivalent radius of a particle;  $\rho$  and  $\rho_s$  are the density of particles and of the suspension respectively;  $\nu$  is the kinematic viscosity; and  $\xi(t)$  is a random perturbation which will further be treated as "white noise."

Corresponding to this equation one can set up a differential equation of the probability density distribution in a random process:

$$\frac{\partial w(t, r)}{\partial t} = \frac{b}{2} \cdot \frac{\partial^2 w(t, r)}{\partial r^2} - \beta \frac{\partial}{\partial r} [r w(t, r)],$$

where

$$b = \frac{b'}{36\pi^2 \rho_s^2 \nu^2 R^2}; \quad \beta = \frac{2R^2 \left( \frac{\rho}{\rho_s} - 1 \right) \omega^2}{9\nu};$$

and  $b'$  is the intensity of random perturbations. The coefficient  $b$  is a measure of disorder in the motion of particles along the vessel under a random perturbation, while  $\beta$  determines the mean rate of particle sedimentation in a centrifugal field.

A solution to this equation for  $w(t, r)$  has been obtained with the initial condition  $w(0, r) = f(r)$  and with the boundary conditions:

$$\frac{b}{2} \cdot \frac{\partial w}{\partial r} - \beta r w = 0 \text{ for } r = r_0; \quad w = 0 \text{ for } r = r_0 + h.$$

The first of these boundary conditions signifies that no particles flow across the wall  $r = r_0$ , while the second one indicates that particles which reached the region boundary  $r_0 + h$  are removed and do not participate further in the sedimentation process.

As a process quality index we use the extracted quantity, i.e., the quantity

$$Q = \frac{1}{\omega_p} \int_{r_0}^r w dr,$$

V. I. Ulyanov (Lenin) Institute of Electrical Engineering, Leningrad. Translated from *Inzhenerno-Fizicheskii Zhurnal*, Vol. 20, No. 5, pp. 940-941, May, 1971. Original article submitted July 28, 1969; revision submitted November 16, 1970.

© 1973 Consultants Bureau, a division of Plenum Publishing Corporation, 227 West 17th Street, New York, N. Y. 10011. All rights reserved. This article cannot be reproduced for any purpose whatsoever without permission of the publisher. A copy of this article is available from the publisher for \$15.00.

which defines the ratio of particles of a given class contained between sections  $r$  and  $r_0$  at an instant of time  $t$  to the number of such particles in the original mixture uniformly distributed along the height of the vessel with the density  $w_p = 1/h$ , where  $h$  denotes the height of the vessel.

Curves representing the process kinetics have been calculated as functions of the parameters  $\bar{h} = h(\beta/b)^{1/2}$  and  $r_0/h$ .

The agreement between calculated and tested data on the constrained sedimentation of abrasive micro-powders in tumbler-type centrifuges has been found satisfactory.